

# HYDRODYNAMIC COMPUTATIONAL EVALUATION IN SOLAR TUBULAR PHOTOBIOREACTORS BENDS WITH DIFFERENT CROSS SECTIONS

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(Received Jun. 08, 2011; Accepted Nov. 02, 2011)

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## ABSTRACT

In this article, the hydrodynamic behavior of a single-phase flow in various solar collectors with different cross sections (circular, octagonal, hexagonal and square), with same hydraulic diameter and longitudinal profile was analyzed. Secondary flow, pressure drop and shear stress were evaluated, because the photosynthetic efficiency and microalgae endurance depend on these properties. These parameters were reviewed at six different culture inlet rates in the collector (from 0,25 m/s to 0,5 m/s), emphasizing in the bends regions. A higher speed and agitation was pre-sent in the square solar collector, contrary to what happened to the circular one. Despite this, the circular solar collector remains the best option for the industrial implementation phase. However, the shear stress generated in the culture -as it passes through the 180° bend of the solar collector- affects the microalgae growth, as stated in the literature.

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**Keywords:** *Computational fluid dynamic, Microalgae, Microalgal biomass, Shear stress, Solar collector, Tubular photobioreactor.*

**Citation:** Ramírez-Duque, J. L. & Ramos-Lucumi, M. A. (2011). Hydrodynamic computational evaluation in solar tubular photobioreactors bends with different cross sections. *CT&F - Ciencia, Tecnología y Futuro*, 4 (4), 59-72.

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## RESUMEN

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**E**n este artículo se analizó el comportamiento hidrodinámico de un flujo monofásico en varios colectores solares, con diferentes perfiles transversales (circular, octagonal, hexagonal y cuadrado), de igual diámetro hidráulico y perfil longitudinal. Se evaluó el flujo secundario, las caídas de presión y el esfuerzo cortante del fluido, ya que de estos depende la eficiencia fotosintética y la vitalidad microalgal. Los anteriores parámetros se revisaron para seis diferentes velocidades de entrada del cultivo en el colector (entre 0,25 m/s a 0,5 m/s) enfatizándose en la región de los codos, donde se presenta una mayor velocidad y agitación en el colector solar cuadrado, contrario a lo que sucede con el circular. A pesar de esto, el colector solar circular continúa siendo la mejor opción en la etapa de implementación industrial. Sin embargo, el esfuerzo cortante que se genera en el cultivo, a medida que atraviesa el codo de 180° del colector solar, afecta el crecimiento de las microalgas, según lo estipulado en la literatura relacionada.

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**Palabras claves:** *Biomasa microalgal, Colectores solares, Dinámica de fluidos computacional, Esfuerzos cortantes, Microalgas, Fotobiorreactor tubular.*

## RESUMO

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**N**este artigo foi analisado o comportamento hidrodinâmico de um fluxo monofásico em vários coletores solares, com diferentes perfis transversais (circular, octogonal, hexagonal e quadrado), de igual diâmetro hidráulico e perfil longitudinal. Foi avaliado o fluxo secundário, as quedas de pressão e o esforço cortante do fluido, já que destes depende a eficiência fotossintética e a vitalidade microalgal. Os anteriores parâmetros foram revisados para seis diferentes velocidades de entrada do cultivo no coletor (entre 0,25 a 0,5 m/s) sendo enfatizado na região dos joelhos, onde é apresentada uma maior velocidade e agitação no coletor solar quadrado, contrário ao que acontece com o circular. Apesar disto, o coletor solar circular continua sendo a melhor opção na etapa de implantação industrial. Porém, o esforço cortante que é gerado no cultivo, a medida que atravessa o joelho de 180° do coletor solar, afeta o crescimento das microalgas, segundo o estipulado na literatura relacionada.

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**Palavras-chaves:** *Biomassa microalgal, Dinâmica de fluidos computacional, Esforços cortantes, Microalgas, Fotobiorreactor tubular.*

## 1. INTRODUCTION

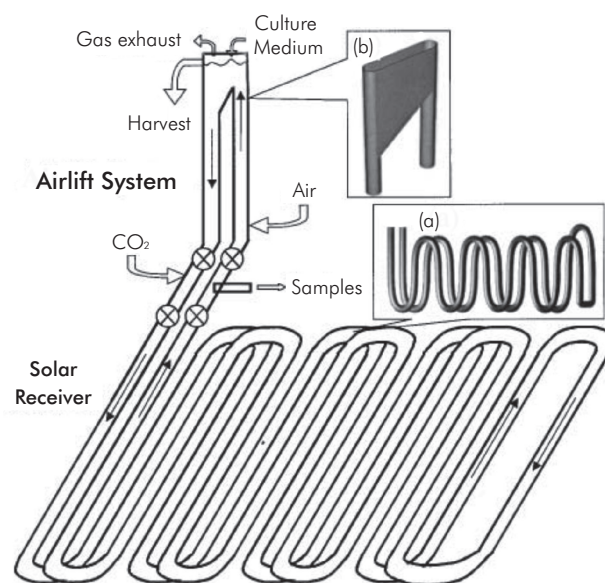
Since the fifties, multiple scientific studies have been carried out to obtain new energy sources from microalgae, with the purpose of replacing fossil fuels and causing less environmental impact (Dyer & Richardson, 1962; Ukeles, 1965). Microalgae also have a large amount of proteins, vitamins and minerals that can be used as raw material in the production of food supplements, organic fertilizers, pharmaceutical products and cosmetics for both human and animal consumption (Harun, Singh, Forde & Danquah, 2011; Mata, Martins & Caetano, 2010; Rawat, Ranjith-Kumar, Mutanda & Bux, 2011; Spolaore, Joannis-Cassan, Duran & Isambert, 2006).

Many countries have implemented the study of microalgae due to their great demand and their suitability as a food source that can compete with traditional agriculture, because their production does not require much water or fertile soil. Even when they are used as biofuels, they are competitive in comparison to those obtained from traditional oily or sweetened plant species as far as performance is concerned. This fact has a positive impact on human and animal food markets. Besides, they do not lead to price increases and other serious problems that traditional plants carry out (Rosello-Sastre, Csögör, Perner-Nochta, Fleck-Schneider & Posten, 2007).

The cultivation of microalgae is found in open systems (ponds, wells, canals, etc) and close systems or photobioreactors (PBR). The latter are characterized by their ability to guarantee optimal conditions for the healthy grow and reproduction of microalgae and cyanobacteria, with the injection of nutrients -such as carbon dioxide, nitrogen and phosphorus- (sunlight or artificial lighting) and the elimination of waste produced by the photosynthesis process, typical of these organisms (Chen, Jiang, An & Yuan, 2009). Among the most widely used PBR's are the tubular photobioreactor (see Figure 1), the bubble column and flat panel photobioreactor. This study will analyze the section of the solar collector of a tubular photobioreactor (TPBR), where the culture medium is found and where the microalgae receive the photonic energy.

For the microalgae to receive the necessary photonic energy to carry out its photosynthetic process and

provide a homogeneous concentration of nutrients that increase the production of biomass, it is necessary to make the mixing of the microalgae culture in the solar collectors of the TFBR. For this process, tools such as static mixers are commonly used (García & Haoulo, 2009; Leeuwner & Eksteen, 2008; Perner-Nochta & Posten, 2007). As an alternative to this mixture system, this work proposes the utilization of noncircular solar collectors. These, together with the curves in the collector, allow certain turbulence levels in the culture medium that could replace the static mixer in the collector of the TFBR, thus decreasing - in comparison to the traditional methods of agitation - the microalgae mortality rate, caused by the shear stress in this section of the TFBR (Camacho-Rubio, Ación-Fernández, Sánchez-Pérez, García-Camacho & Molina-Grima, 1999; Schneiderbauer & Pirker, 2010).



**Figure 1.** Tubular photobioreactor scheme with Airlift system. Taken from Ación-Fernández, Fernández-Sevilla, Sánchez-Pérez, Molina-Grima and Chisti (2001).

Retaking research done on the flow in sections or curved ducts, Rowe (1970) revealed that the water flow presents the maximum increase in the secondary flow when it enters the 180°-curvature. Azzola, Humphrey, Iacovides & Launder (1986) noticed that the flow speed increases notably while crossing the curvature due to pressure associated with the main flow, which generates the secondary flow in the duct. Khalid, Legrand & Rosant (1996) highlighted the curves influence in the speed profiles, which confirms that the resulting flow is explained by the coupling between the effects of the curves (acceleration and deceleration of the

fluid entering the curvature). Sudo, Sumida and Hibara (2000) showed that the high speed region is located in the 90°-section in a 180° elbow and this occurs thanks to the secondary flow and the turbulence level present in this area

The interest in the flows study in curved tubes stems from its wide range of applications in engineering (for example, hydraulic piping systems related to corrosion) and the dynamics of biofluids, such as the blood flow in the vascular system, where the distribution of speed, pressure, and shear stress can help to understand arterial disorders such as atherosclerosis (Santamarina, Weydahl, Siegel & Moore, 1998; Arada, Pires & Sequeira, 2007). Previous generalized studies have been conducted on the behavior of a fluid in curved ducts. One such study by Zhang, Zhang and Jü (2001) found that in rectangular ducts, four types of secondary vortex coexist and they produce a variation of the secondary flow and the main axial flow in the duct (vortices due to centrifugal force, Coriolis force, centrifugal instability and Coriolis instability). Huttel and Friedrich (2000 and 2001) demonstrated that the amounts of flow were affected by the curvature of helical spiral pipe because the secondary flow induced by the curvature leads to an increase of the kinetic energy and a fluctuation of the dissipation rate, while Ma, Shen, Zhang and Zhang (2006) discovered that the laminar flow rotation in the curve input region of a duct influences the flow structure and the friction factor. The secondary flow appears in the early stage of the development and then becomes the vortex structure. Yamamoto, Akita, Ikeuchi, & Kita, (1995) and Chang, Chiang and Chou (2010) worked in hexagonal ducts; the first ones for establishing the destabilizing effect on the flow due to the torques generated and the last ones have reported the influence of this profile in the heat transfer and the pressure drop.

However, no advances have been recently published about the microalgae cultivation in a FBRT, which are focused on the collector curvature where the critical area is located and the influence of uncommon geometries is considered for the solar collector (square, hexagonal and octagonal) in the agitation of the cultivation. Taking into account the neutral buoyancy of the algae in the culture medium (Michels, van der Goot, Norsker & Wijffels, 2010), this article analyzes the development of a single phase flow -water- through horizontal ducts of different profile (circular, octagonal, hexagonal and square) using the computational tool of Dynamic Fluids (CFD) called FLUENT 12.1.2, under the Reynolds stress model.

## 2. THEORETICAL FRAMEWORK

### Turbulence Models

The turbulence models  $k$ -epsilon ( $k$ - $\epsilon$ ) and Reynolds stress (RSM) are the most used models for establishing the behavior of this type of flow and are based on the continuity equations of average momentum (Bitog *et al.*, 2011). The  $k$ - $\epsilon$  model is simple, numerically robust and easy convergence, but it is known to generate poor results for flow with high agitation or a large amount of vortices. Meanwhile, the RSM is more appropriate for this type of simulations although it require machines with more powerful computational characteristics and can present stability problems (Shalaby, Pachler, Wozniak, & Wozniak, 2005).

The Reynolds Stress Model (RSM) is a detailed prototype of turbulence that provides better approximations to the true flow behavior (Alpma & Long, 2005; Fernández-Roque, Toledo-Velásquez & Vásquez-Flores, 2006). The RSM is used for calculating the Reynolds stress from the differential transport equations, represented in the Equation 1 (Alpma & Long, 2005; Fernández-Roque *et al.*, 2006).

$$\frac{\partial}{\partial t}(\rho \overline{u_i u_j}) + \frac{\partial}{\partial x_k}(\rho u_k \overline{u_i u_j}) = P_{ij} + F_{ij} + D_{ij}^r + \phi_{ij} - \epsilon_{ij} \quad (1)$$

In Equation 1, the term on the left is known as the convection term,  $C_{ij}$ ;  $P_{ij}$ , from which the stress production is deduced:

$$P_{ij} = -\rho \left( \overline{u_i u_k} \frac{\partial u_j}{\partial x_k} + \overline{u_j u_k} \frac{\partial u_i}{\partial x_k} \right) \quad (2)$$

$F_{ij}$  represent the rotation:

$$F_{ij} = -2 \rho \Omega_k \left( \overline{u_i u_m} \epsilon_{ikm} + \overline{u_i u_m} \epsilon_{jkm} \right) \quad (3)$$

The turbulent diffusion is indicated by  $D_{ij}^T$ :

$$D_{ij}^r = -\frac{\partial}{\partial x_k} \left[ \overline{\rho u_i u_j u_k} + p(\delta_{kj} u_i + \delta_{ik} u_j) \right] \quad (4)$$

$\phi_{ij}$  symbolizes the correlation between the pressure and the deformation:

$$\hat{p}_{ij} = + \left( \overline{\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i}} \right) \quad (5)$$

$\varepsilon_{ij}$  is the turbulence dissipation:

$$\varepsilon_{ij} = -2\mu \left( \overline{\frac{\partial u_i}{\partial x_k} \frac{\partial u_j}{\partial x_k}} \right) \quad (6)$$

**Shear Stress**

The hydrodynamic forces present in a FBRT solar collector may cause high shear stress that affects the microalgae (Mazzuca-Sobezuk, García-Camacho, Molina-Grima & Chisti, 2006; Sánchez-Mirón, García-Camacho, Contreras-Gómez, Molina-Grima & Chisti, 2000), reducing its growth or causing its cellular death. However, this agitation movement in the cultivation is necessary for the microalgae to remain in suspension and for improve the light distribution (Michels *et al.*, 2010). This shear stress, present in the solar collector, is directly related to the viscosity of the culture medium and the strain rate, as shown in Equation 7 (Mott, 2005).

$$\tau = \mu \frac{\partial u}{\partial y} \quad (7)$$

Where  $\tau$  is the Shear Stress,  $\mu$  is the viscosity of the fluid;  $u$  is the fluid speed and  $y$  is the coordinate perpendicular to the direction of flow.

**3. METHODOLOGY**

The present study aims at establishing a suitable methodology and a complete validation of the initial data to obtain an appropriate simulation of the culture

medium in the solar collector of the FBRT. For this purpose, the main parameters are speed, agitation and shear stress present in the flow.

**Geometry**

The hydraulic diameter, the curvature and the length of these pipes are the only factors that remain constant for the different profiles. Therefore, it is necessary to establish the general dimensions of each one of the studied profiles (see Figure 2). In the case of the circular duct, the hydraulic diameter corresponds to the diameter of the profile. However, for the other configurations, the hydraulic diameter,  $D_h$ , is given by Equation 8 (Aparecido & Cotta, 1990) which relates the cross sectional area (A) with the wet perimeter ( $P_{wet}$ ) of the duct. See Table 1.

**Mesh Generation**

The RSM equations are an adequate mathematical representation of the flows, even the turbulent ones.

However, the resolution of these equations for the calculation of the turbulent flow requires for a temporary discretization and a fine mesh calculation. For this reason, the generation of the mesh is the initial step in the simulations CFD.

This work relies on a section of the solar collector of the FBR as a simulation object. The non-structured three dimensional mesh used in these sections of the ducts has more than 600 000 nodes totally (see Table 2) and was created with the software ICEM CFM (ANSYS 12.1). See Figure 3.

$$D_h = 4A / p_e \quad (8)$$

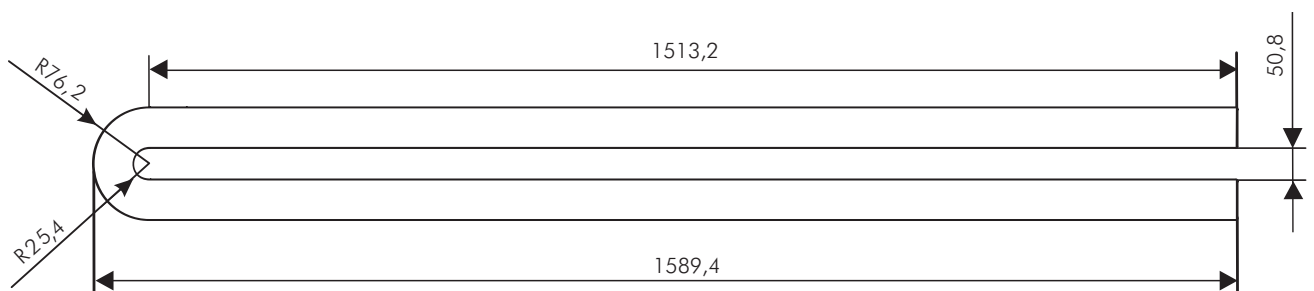


Figure 2. General dimensions of the solar collector for the different sections (dimensions in mm).

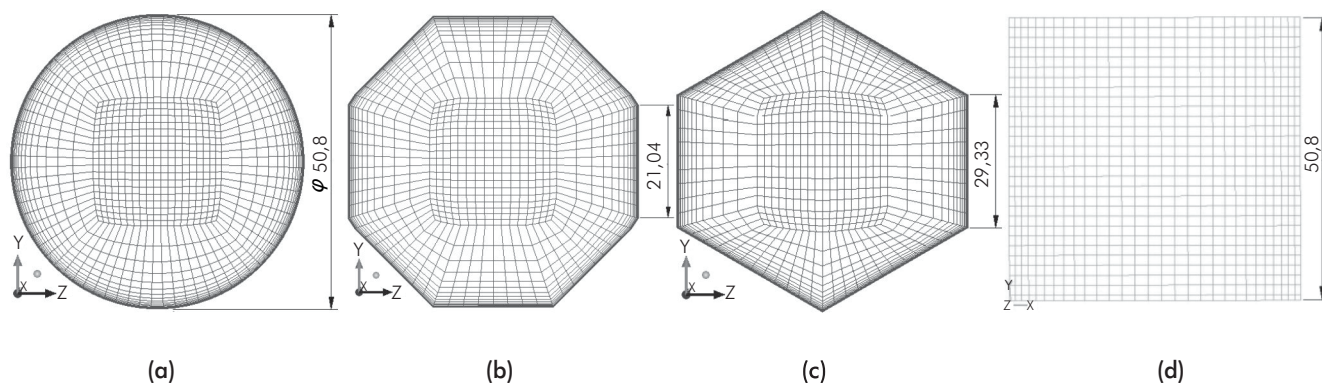


Figure 3. Cross mesh of the ducts for the (a) circular, (b) octagonal, (c) hexagonal and (d) square sections. Measures in mm.

**Initial Conditions And Simulation**

The numerical simulation of the monophasic flow (water) in the ducts was performed by using the FLUENT software version 12.1.2. (Ansys Inc.). The workplace was a Dell™ Precision™ M6500 laptop computer with an Intel Core i7 quad-core processor of 1.6 GHz. The time of calculation of each one of the 24 simulations was two hours, approximately.

Due to the small size of the bubbles that are generated by the injection of carbon dioxide in the horizontal solar collector, a homogeneous flow is assumed in this situation (Camacho-Rubio *et al.*, 1999). The laminar flow was analyzed under a stationary state with implicit formulation through the Reynolds Stress Model (pressure - linear deformation), using different fluid inlet velocity in all the ducts (see Table 2) and a turbulence intensity of 10%. The condition at the entrance of the ducts is velocity. For the output, it is pressure equal to  $\Delta P$ .

The fluids turbulence in these collectors is significantly affected by the walls. Therefore, the mesh dependence in this analysis also stems from the fact

that the gradient near the walls should not be very big (Salim & Cheah, 2009).

In order to guarantee the validity of the obtained results, the parameters that affect the numerical resolution of the problem should be controlled. It is possible to act on the iterative process by defining the types of discretization, varying the relaxation factors and setting the finalization criteria of the iterations. (Aparecio & Cotta, 1990).

Table 1. Geometry, number of nodes and initial conditions for the simulation of the different solar collectors of a FBR.

	Circle	Octagon	Hexagon	Square
Dimensions [mm]	50,80	21,04	29,33	50,80
No. Nodes	923,844	785,960	648,016	860,400
Analysis	Stationary state			
Formulation	Implicit			
Model	Reynolds stress			
Model type	Pressure - lineal deformation			
Fluid	Monophasic (water)			

Table 2. Flow inlet velocity in the ducts with their corresponding Reynolds numbers (Fluid: Water).

Velocity inlet (m/s)	0,25	0,30	0,35	0,40	0,45	0,50
Reynolds Number	12,677	15,212	17,748	20,283	22,818	25,354

**4. RESULTS AND DISCUSSION**

The main interests of this study are the changes in the speed, the pressure drop along the duct curvature and the development of the secondary flow according to the geometry. This is due to the dependence that these factors have on the losses produced by the fluid friction on the duct walls and also the dependence on the shear stress generated by the fluid on the algae, which can cause cellular damage. Tables 3, 4 and 5 show the maximum speeds reached by the fluid within the duct and the pressure at the entrance of the ducts (maximum pressure) and the maximum magnitude of the secondary flow, respectively.

In order to identify the fluid behavior in the curvature of the solar collector for the different profiles, this elbows section has been fragmented in 5 parts. See Figure 4.

**Table 3.** Maximum speed in the different ducts.

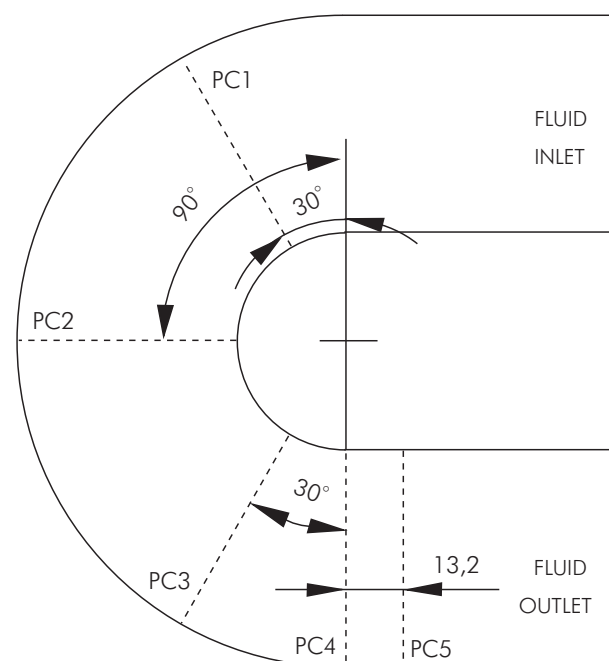
$V_{max}$ (m/s)	Circle (m/s)	Octagonal (m/s)	Hexagonal (m/s)	Square (m/s)
0,25	0,366	0,365	0,377	0,414
0,30	0,439	0,440	0,454	0,495
0,35	0,511	0,516	0,530	0,575
0,40	0,584	0,592	0,606	0,655
0,45	0,657	0,669	0,682	0,730
0,50	0,731	0,745	0,758	0,812

**Table 4.** Pressure drop in the different ducts.

$V_{inlet}$ (m/s)	Circle (Pa)	Octagonal (Pa)	Hexagonal (Pa)	Square (Pa)
0,25	130,2	115,0	107,2	81,8
0,30	176,7	151,1	140,3	107,9
0,35	228,6	189,7	175,9	137,9
0,40	285,4	231,1	213,9	172,5
0,45	346,7	274,8	254,0	216,6
0,50	412,4	321,0	296,4	263,1

**Table 5.** Maximum secondary flows in the different ducts.

$V_{inlet}$ (m/s)	Circle (m/s)	Octagonal (m/s)	Hexagonal (m/s)	Square (m/s)
0,25	0,342	0,328	0,340	0,386
0,30	0,409	0,390	0,408	0,463
0,35	0,476	0,454	0,475	0,534
0,40	0,543	0,518	0,543	0,612
0,45	0,610	0,582	0,610	0,690
0,50	0,676	0,645	0,677	0,768



**Figure 4.** Visualization of the planes positions in the elbows (mm).

The acceptance of the obtained results can be examined through diverse numerical studies or by comparison to the experimental data.

**Speed**

The flow speed makes it possible to predict the fluid behavior in the ducts and to establish the critical situations of the process. In this study, the speed development was completed before 0,5 m of the entrance of the fluid in the ducts, long before the elbow beginning, which

makes it possible to establish the typical features of the fluid when entering the curvature of the duct as is shown in Figure 5.

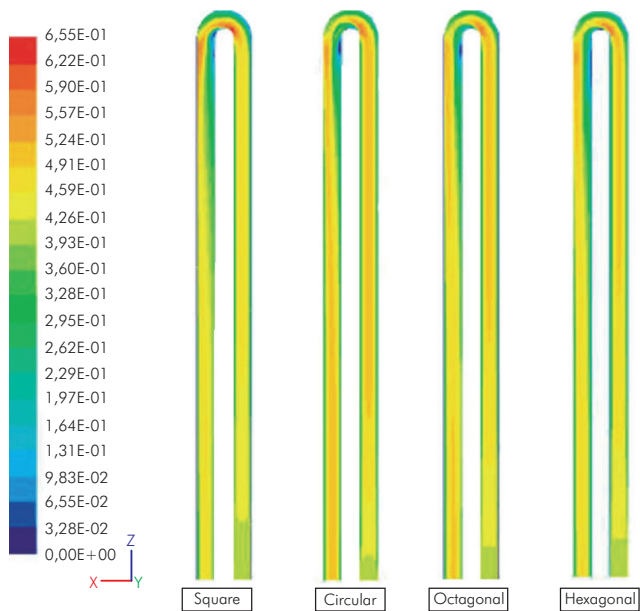


Figure 5. Comparison of the speed profiles of the central longitudinal plane of the duct for  $V_{entrance} = 0,40$  m/s.

Figure 6 shows the speed contour profile of the different types of solar collectors on a plane located in the center of the elbow curvature (PC2) when the fluid entrance speed in all the collectors is 0,4 m/s; while Figure 7 shows the speed vectors in five different positions in the curvature (see Figure 4) when the fluid entrance speed in all the collectors is 0,4 m/s. The right side of each image represents the internal zone of the curvature.

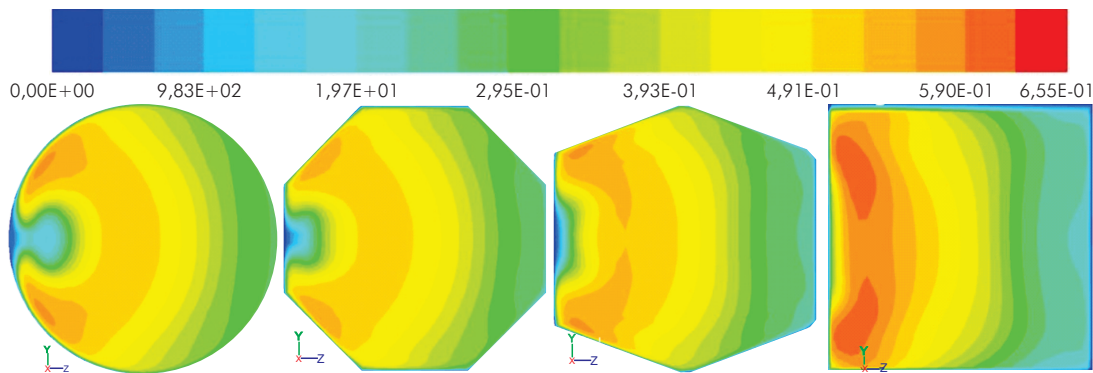


Figure 6. Profile of speed contours of the plane across the duct in the middle of the curvature in the four profiles for  $V_{inlet} = 0,4$  m/s. (PC2).

### Secondary Flow

The resistance due of the friction of the ducts walls and the action of the centrifugal force produce a rotation in the fluid movement known as secondary flow; this movement is perpendicular to the axis of the pipe and is opposed to the axial movement of the flow (Belt, Van't Westende, Portela, Mudde & Oliemans, 2004; Molina-Grima, Ación-Fernández, García-Camacho & Chisti, 1999).

Figure 8 shows the secondary flow for each of the profiles when the water entrance speed is 0,4 m/s.

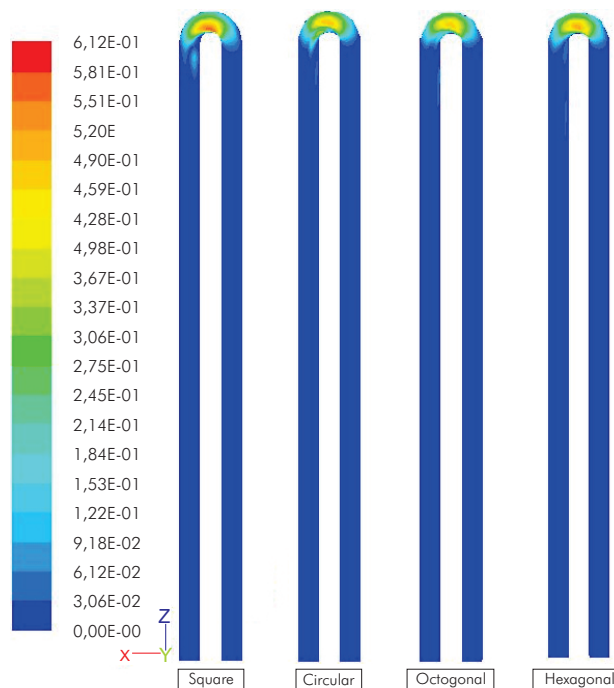


Figure 8. Contour of the secondary flow in a plane ( $z = 2,54$  m) across the ducts.



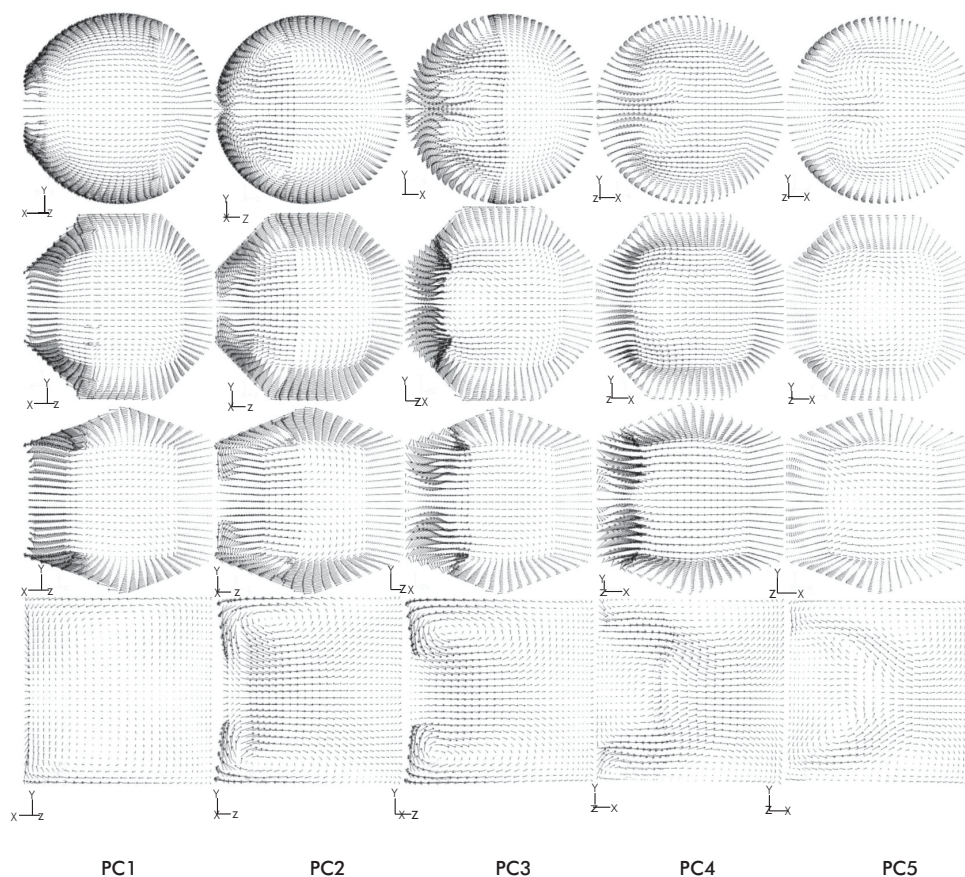


Figure 7. Speed vectors of the plane across the duct. Several positions of the curvature for the four profiles for  $V_{inlet}=0,4$  m/s.

The secondary flow is related to the agitation of the fluid in the duct due to the rotation of the flow, which explains the behavior of the fluid in the curvature of the collector.

### Shear Stress

Algae's tolerance to shear stress depends specifically on the species of microalgae. *Chaetoceros muelleri*, in particular, can endure 1,8 Pa without presenting changes in the growing process (Michels *et al.*, 2010); the growth of the microalgae *Spirulina platensis* undergoes a change when affected by a shear stress higher than 0,3 Pa (Mitsuhashi, Hosaka, Tomonaga, Muramatsu, & Tanishita, 1995) but no significant cellular damage is produced. While, for the highly sensitive *Protoceratium reticulatum* microorganism, a damage threshold was observed at an average shear stress of approximately 0,16 mPa (García-Camacho *et al.*, 2007); for *Phaeodactylum tricornutum*, a shear stress value of 7 Pa led to the highest growth rate caused by a balance between mass transfer limitations and shear damage (Contreras, García, Molina & Merchuk, 1998).

Table 6 shows the maximum shear stress that the flow reaches in each of the ducts. The shear stress is directly related to the fluid viscosity (Hämäläinen, 2001; Ugwu, Ogbonna & Tanaka, 2005; Wu & Merchuk, 2004), and is higher near to the walls of the ducts. Figure 10 illustrates this phenomenon in the collectors when the speed of entrance is 0,4 m/s.

Table 6. Maximum shear stress magnitude regarding the inlet velocity in the different ducts.

$V_{inlet}$ (m/s)	Circle (Pa)	Octagonal (Pa)	Hexagonal (Pa)	Square (Pa)
0,25	1,215	0,977	0,810	0,445
0,30	1,611	1,219	1,023	0,454
0,35	2,026	1,496	1,240	0,561
0,40	2,470	1,767	1,459	0,536
0,45	2,942	2,046	1,676	0,545
0,50	3,429	2,317	1,902	0,550

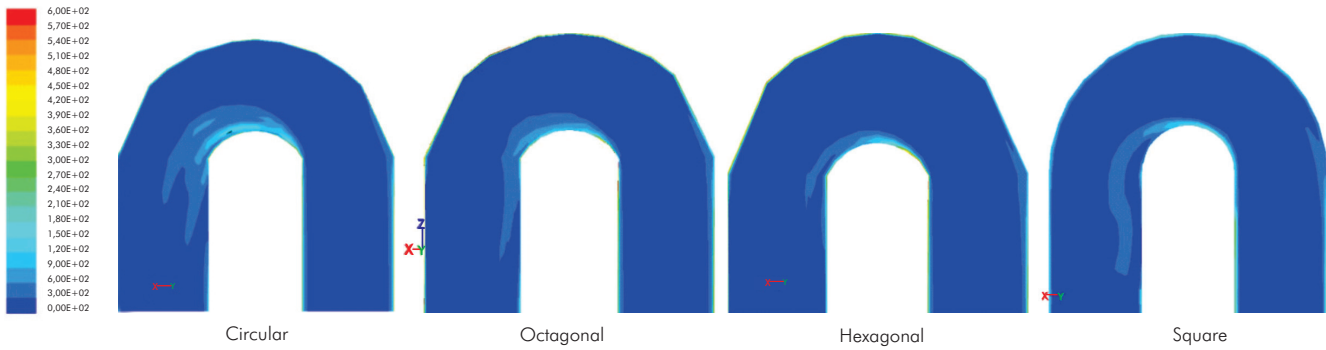


Figure 9. Profiles for the strain rate of the plane longitudinal to the duct in the middle of the curvature for the four profiles when  $V_{inlet} = 0,4$  m/s.

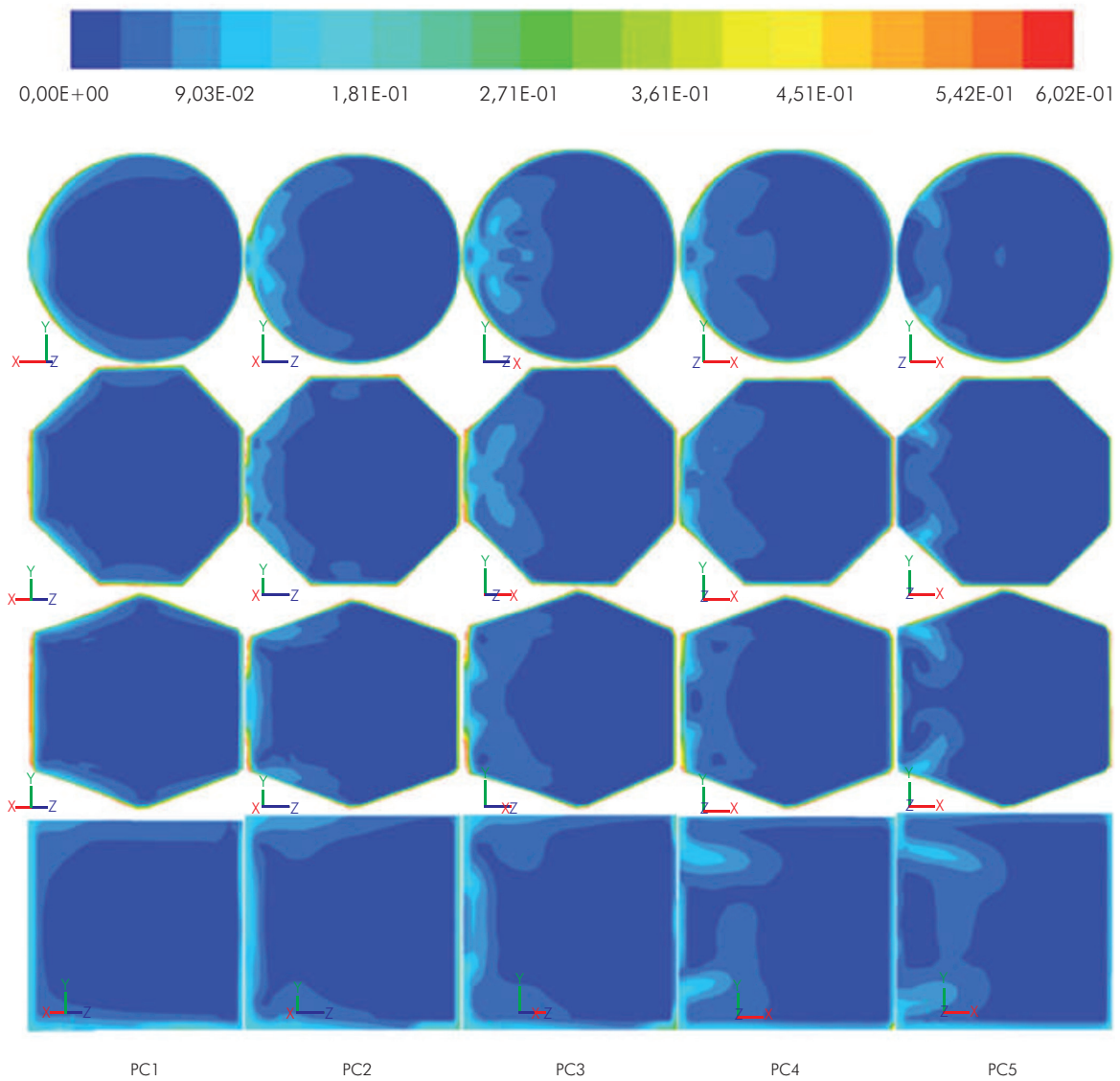


Figure 10. Shear stress profiles in different planes of the duct for the three profiles when  $V_{inlet} = 0,4$  m/s.

## 5. CONCLUSIONS

- According to the results, it is possible to establish a parameter of duct selection for transporting fluids such as the microalgae cultivation according to the axial and rotational movements that are required and the change of pressure. The square profile is the most critical case among the collectors, mainly in the curved zone. This guarantees the constant movement of the fluid and the diminution of the sealing effect of the algae in the collectors.
- Since the pressure drop is affected by the fluid speed, it determines the direction and the movement of the flow in the duct. The secondary flow is generated from the high pressure region to the low pressure region (Yue, Dooley & Feng, 2008). This flow dissipates after the fluid leaves the elbow, as presented by Azzola *et al.* (1986) and Sudo *et al.* (2000) in their works. This situation can be seen in Tables 4 and 5, in which the higher pressure drop occurs in the circular profile. Similarly, the highest secondary flow occurs in comparison to other profiles.
- It should be noticed in Table 3 that the flow can reach a higher speed in the duct with a square profile than in the other ducts (Figure 5). This is due to the vortex intensity before initiating the curvature, since it is inversely related to the entrance speed of the flow into the elbow (Pruvost, Legrand & Legentilhomme, 2004). According to Figure 5, the flow is not totally developed in the square profile, contrary to what happens in the circular profile. When it enters the elbow, the fluid speed is higher in the internal section, which leads to a higher drop in speed at the exit of the internal section of the elbow, due to the vortices that originate here thanks to the change in speed within the elbow (Sudo *et al.*, 2000).
- The maximum shear stress that occurs in the flow should not exceed the maximum shear stress withstood by the cultivation, as the development and growth of the microalgae would be put at risk. Each type of algae tolerates a certain magnitude of shear stress, such as *Chaetoceros muelleri*, which can withstand 1,8 Pa without presenting changes in its growing process (Michels *et al.*, 2010). Therefore, for microorganisms highly shear sensitive like the *Protoceratium reticulatum*, low speeds should be used for the entrance of the cultivation medium into the solar collector.

Although the solar collector with square profile presents the best features as far as shear stress and agitation are concerned, its weakness is its difficult manufacture. It is feasible to use a circular profile solar collector, which ensures low speed of the culture when it enters the collector, thus avoiding the presence of shear stress that are harmful to microalgae.

## ACKNOWLEDGMENTS

The author of this work is grateful to the Research Direction at *Universidad Autónoma de Occidente*, for the funding of the project “Design of a Photobioreactor Prototype for the Production of Biomass from Algae as a Cleaner Source of Energy in Valle del Cauca.”

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## NOTATION

$A$	Cross sectional area
$D^T$	Turbulent diffusion
$F$	Rotation
$p$	Pressure
$P$	Stress production
$p_{wet}$	Wet perimeter
$\overline{u_i u_k}$	Reynolds stress tensor
$u_{i,j,k}$	Fluctuating velocity in $x, y, z$ direction
$\delta$	Boundary layer thickness
$\varepsilon$	Dissipation
$\Phi$	Correlation between pressure and deformation
$\mu$	Dynamic viscosity
$\rho$	Density
$\Omega_{l, \varphi, \kappa}$	Vorticity component in $x, y, z$ direction