

Preferential solvation of triclin in {ethanol (1) + water (2)} mixtures at several temperatures

Juan José Sandoval-Castro¹, Claudia Patricia Ortiz², Juan Diego Rodríguez-Rubiano³, Gerson Andrés Rodríguez-Rodríguez⁴, Daniel Ricardo Delgado^{1*}

¹ Grupo de Investigaciones GRIAUCC, Programa de Ingeniería Industrial, Facultad de Ingeniería, Universidad Cooperativa de Colombia, Neiva, Colombia, calle 11 No. 1-51, Neiva Huila, Colombia.

* E-mail: danielr.delgado@campusucc.edu.co.

² Grupo de Investigaciones en Seguridad y Salud en el Trabajo - FET, Programa de Administración de la Salud Ocupacional, Fundación Escuela Tecnológica de Neiva, Km. 11 vía al Sur, Neiva-Rivera, Colombia.

³ Programa de Ingeniería Industrial, Facultad de Ingeniería, Universidad Antonio Nariño, sede Buganviles, calle 19 No. 42-98, Neiva Huila, Colombia.

⁴ Grupo de Investigaciones Farmacéutico-Físicoquímicas, Departamento de Farmacia, Facultad de Ciencias, Universidad Nacional de Colombia, sede Bogotá, Cra. 30 No. 45-03, Bogotá, D. C., Colombia.

Received: January 22, 2018

Accepted: February 23, 2018

SUMMARY

The preferential solvation parameters of triclin in {ethanol (1) + water (2)} binary mixtures were obtained from their thermodynamic properties by means of the inverse Kirkwood-Buff integrals method. Triclin is very sensitive to specific solvation effects, so the preferential solvation parameter by ethanol (1), $\delta x_{1,3}$, is negative in the water-rich mixtures but positive in all the other compositions at temperatures from 293.15, to 313.15 K. It is conjecturable that in water-rich mixtures the hydrophobic hydration around the aromatic and methyl groups of the drug plays a relevant role in the solvation. The higher drug solvation by ethanol in mixtures of similar solvent proportions and in ethanol-rich mixtures could be due mainly to polarity effects. In these mixtures, the drug would be acting as Lewis acid with the ethanol molecules because this co-solvent is more basic than water.

Key words: Triclin, IKBI, ethanol, preferential solvation.

RESUMEN

Solvatación preferencial de tricina en mezclas etanol + agua a varias temperaturas

Los parámetros de solvatación preferencial del tricina en mezclas {etanol (1) + agua (2)} se obtuvieron a partir de las propiedades termodinámicas de solución, mediante el método de las integrales inversas de Kirkwood-Buff. La tricina es muy sensible a los efectos de solvatación específicos, por lo que el parámetro de solvatación preferencial, $\delta x_{1,3}$, es negativo en las mezclas ricas en agua, pero positivo en todas las otras composiciones a temperaturas desde 293,15 hasta 313,15 K. Se puede establecer que en mezclas ricas en agua la hidratación hidrofóbica alrededor de los grupos aromáticos y metilo del fármaco tiene un papel relevante en la solvatación. La mayor solvatación del fármaco por etanol se presenta en mezclas de proporción intermedia y en mezclas ricas en etanol, esto podría deberse principalmente a los efectos de la polaridad. En estas mezclas, el fármaco actuaría como ácido de Lewis con las moléculas de etanol, puesto que este codisolvente es más básico que el agua.

Palabras clave: Tricina, IKBI, etanol, solvatación preferencial.

INTRODUCTION

Tricin (5,7-dihydroxy-2-(4-hydroxy-3,5-dimethoxyphenyl)chromen-4-one) (Figure 1) is a flavone often found in the outer layer of cereal crops, has also been associated with reduction in cancer. In a mouse model of intestinal cancer, addition of tricetin to the diet (0.2%, which was about 6 mg per mouse per day) resulted in 33% fewer intestinal adenomas [1]. In another study, dietary tricetin was found to inhibit inflammation-induced colon cancer in mice [2]. Additional beneficial health effects of tricetin are summarized in a recent review [3].

In foods tricetin is mainly found in whole cereal grains, such as rice, barley, oat, and wheat, also, in medicinal plants such as *Artemisia copa* [4]. However, higher levels of tricetin and its derivatives are often found in other nonedible tissues, such as leaves and grain hulls. Because of the potential therapeutic use of tricetin and its derivatives, extraction from such nonedible sources has been proposed [5]. Tricetin has also recently been found as a component of lignin in some species, particularly monocots [6].

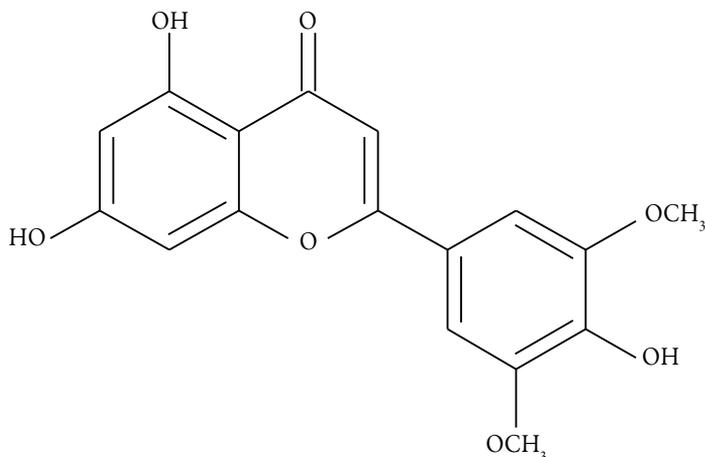


Figure 1. Molecular structure of tricrin.

Within the context of this article, the studies of the solubility of drugs in solvent mixtures have as their purpose the modeling of the solubilities, with the aim of reducing the number of experimental tests, and in the best case, to bring them to zero [7-12]. Cheng *et al.* [13] determined the solubility of Tricrin in {ethanol (1) + water (2)} cosolvent mixtures at different temperatures. Some thermodynamic functions associated to the dissolution of this drug were obtained, but nothing about the drug is preferentially solvated by water and by ethanol in the aqueous solvent mixtures. Nevertheless, more insight into the interactions of the drug molecules with those of the components of the mixed solvent would help in the choice of better co-solvents for the enhancement of drug solubilities in aqueous media [14-16].

The professor Marcus addressed this problem by means the inverse Kirkwood-Buff integral (IKBI) method [17,18]. Where the results are expressed in terms of the preferential solvation parameter $\delta x_{3,1}$ for the solute tricrin (3) by the component solvents ethanol (1) and water (2):

$$\delta x_{1,3} = x_{3,1}^L - x_1 = -\delta x_{2,3} \quad (1)$$

where $\delta x_{3,1}$ is the local mole fraction of 1 in the surroundings of the solute 3 and x_1 is its mole fraction in the bulk solvent mixture. 3 is preferentially solvated by 1 when $\delta x_{3,1} > 0$, otherwise by 2. Negligible preferential solvation is indicated when $|\delta x_{3,1}| \leq 0.01$, but values $\delta x_{3,1} \approx x_2$ signify $\delta x_{3,1} \approx 1$ or complete selective solvation of 3 by 1. The magnitude and shape of the $\delta x_{3,1} = f(x_1)$ curve provide the desired information on the relative strength of the interactions of 3 with 1 and with 2 in their mixture.

In order to apply the IKBI method, the solubility data need to be transformed into standard molar Gibbs energies of transfer from one of the components, say 2, into the mixture 1+2. If x_2 is the solubility as a function of the solvent composition, then:

$$\Delta_{tr}G_{3,2 \rightarrow 1+2}^{\circ} = RT \ln \left(\frac{x_{3,2}}{x_{3,1+2}} \right) \quad (2)$$

THEORETICAL

Preferential solvation

The IKBI approach depends on obtaining the Kirkwood-Buff integrals as follows [17-22]

$$G_{1,3} = RT\kappa_T - V_3 + x_2V_2D/Q \quad (3)$$

$$G_{2,3} = RT\kappa_T - V_3 + x_1V_1D/Q \quad (4)$$

Here $G_{1,3}$ and $G_{2,3}$ are the Kirkwood-Buff integrals (in $\text{cm}^3 \text{mol}^{-1}$) as obtained from the thermodynamic data: the isothermal compressibility of the solvent mixtures, κ_T (in GPa^{-1}), and standard partial molar volume of solute in this mixture, V_3 (in $\text{cm}^3 \text{mol}^{-1}$). The functions

D and Q (in kJ mol^{-1} , as is RT) are given in equations (5) and (6), and depend on the first derivative of standard molar Gibbs energies of transfer, $\Delta_{tr}G^{\circ}$, and the second derivative of the excess Gibbs energy of mixing of the two solvents, G_{1+2}^E , with respect to the composition [23, 24].

$$D = \left(\frac{\partial \Delta_{tr}G_{(3,2 \rightarrow 1+2)}^{\circ}}{\partial x_1} \right)_{T,p} \quad (5)$$

$$Q = RT + x_1x_2 \left[\frac{\partial^2 G_{1+2}^E}{\partial x_2^2} \right]_{T,p} \quad (6)$$

A final quantity that is required is the correlation volume around 3, V_{cor} , within which preferential solvation takes place and the local mole fraction, $x_{1,3}^L$, is defined [18, 25].

$$V_{cor} = 2522.5 \left[r_3 + 0.1363 \sqrt[3]{(1 - x_{1,3}^L)V_2 + x_{1,3}^L V_1 - 0.085} \right]^3 \quad (7)$$

This volume involves one solvation shell and depends on the size of the solute molecule (its radius, r_3 in nm, equation 8) plus a distance of one mean solvent diameter from the surface of the solute.

$$r_3 = \sqrt[3]{\frac{3 \times 10^{21} V_3}{4\pi N_A}} \quad (8)$$

The resulting correlation volume, in $\text{cm}^3 \text{mol}^{-1}$, the numerical coefficients of which relate sizes to volumes, requires iteration, since it involves the local mole fractions of the two solvents.

Finally, the resulting preferential solvation parameter is then:

$$\delta x_{3,1} = \frac{x_1 x_2 (G_{1,3} - G_{2,3})}{x_1 G_{1,3} + x_2 G_{2,3} + V_{cor}} \quad (9)$$

However, the correlation volume requires iteration, because it depends on the local mole fractions [19, 26, 27].

RESULTS AND DISCUSSION

The experimental solubility of tricrin (3) in {ethanol (1) + water (2)} mixtures (Fig. 2) was taken from the literature [13].

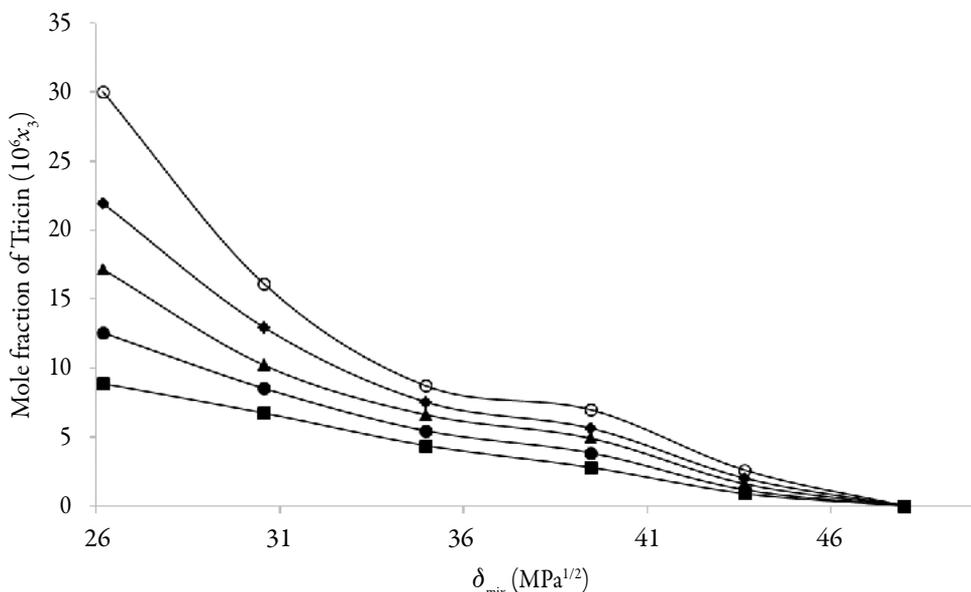


Figure 2. Experimental molar solubility of Tricrin in {ethanol (1) + water (2)} mixtures at different temperatures; (■)=293.15 K; (●)=298.15 K; (▲)=303.15 K; (◆)=308.15 K; (○)= 313.15 K). Data taken from Cheng *et al.* (2016) [6]. ($10^6 x_3$).

The solubility increases with temperature in all cases indicating that the dissolution process is endothermic. The highest solubility of triclin (3) expressed as a mole fraction were obtained in near ethanol (1) at $T = 313.15$ K, whereas the lowest values were found in pure water (2) at 293.15 K (Figure 2).

On the other hand, Fig. 2 depict the solubility profiles as a function of the polarity of the mixtures, expressed by their solubility parameters (δ_{mix}). For a binary mixture δ_{mix} is calculated from the solubility parameters of the pure solvents ($\delta_1 = 26.5 \text{ MPa}^{1/2}$ and $\delta_2 = 47.9 \text{ MPa}^{1/2}$ [28, 29]).

The solubility parameter of solute, estimated according to the groups contribution method proposed by Fedors [21], is $\delta_3 = 34.44 \text{ MPa}^{1/2}$ (Table 1). Usually, the maximum solubility of a substance is found in a solvent or mixture of solvents with polarity similar to that of the solute. This behavior has been described by Delgado and Martinez in several investigations [30-37]. However, the experimental data did not present a maximum in a mixture but in pure ethanol (1).

Table 1. Application of the Fedors' method to estimate internal energy, molar volume, and Hildebrand solubility parameter of Tricin (3).

Group	Group number	$V(\text{cm}^3 \text{ mol}^{-1})$	$U(\text{kJ mol}^{-1})$
-CH ₃	2	2×33.5	1×4.71
>C=O	1	1×10.8	1×17.4
>C=	1	1×-5.5	1×4.31
-CH=	1	1×13.5	1×4.31
-OH	3	3×10	3×29.8
-O-	3	3×3.8	3×3.35
Phenyl (tetrasubstituted)	2	2×14.4	2×31.9
Ring closure	1	1×16.00	1×1.05
Conjugate bond	1	1×-2.2	1×1.67
	Total	169.8	201.4
	Solubility parameter	$(201410/169.8)^{1/2}$	$34.44 \text{ MPa}^{1/2}$

Preferential solvation

Standard molar Gibbs energy of transfer of triclin from neat water to {ethanol (1) + water (2)} mixtures is calculated and correlated to a non-regular polynomial from the

drug solubility data by using equation (10). Figure 3 shows the Gibbs energy of transfer behavior at 323.15 K. Thus, the coefficients of the polynomials are shown in Table 2.

$$\Delta_{tr}G_{3,2 \rightarrow 1+2}^0 = RT \ln \left(\frac{x_{3,2}}{x_{3,1+2}} \right) = a + bx_1 + cx_1^{1.5} + dx_1^2 + ex_1^{2.5} \quad (10)$$

Table 2. Coefficients of the equation (10) applied to the Gibbs energy of transfer of tricrin (3) from neat water (2) to {ethanol (1) + water (2)} mixtures at several temperatures.

Coefficient kJ mol ⁻¹	293.15 K	298.15 K	303.15 K	308.15 K	313.15 K
<i>a</i>	0.00029	0.0023	0.0018	0.0032	0.0052
<i>b</i>	-289.49	-282.36	-281.80	-285.37	-282.00
<i>c</i>	722.40	683.54	675.90	706.07	697.87
<i>d</i>	-685.23	-624.59	-606.21	-654.99	-644.01
<i>e</i>	230.18	200.83	189.39	211.88	205.75

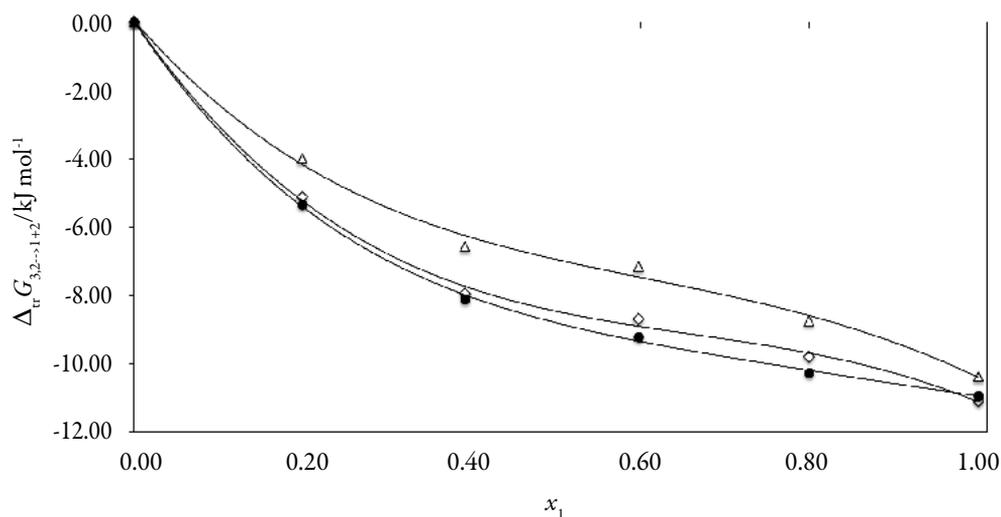


Figure 3. Gibbs energy of transfer of tricrin (3) from neat water (2) to {ethanol (1) + water (2)} co-solvent mixtures at some temperatures (●=293.15 K; ◇=303.15 K; △=313.15 K).

Thus *D* values are calculated from the first derivative of polynomial models (Equation 11) solved according to the co-solvent mixtures composition. This procedure was done varying by 0.05 in mole fraction of methanol but in the following tables the respective values are reported varying only by 0.10.

$$D = \left(\frac{\partial \Delta_{tr} G_{(3,2 \rightarrow 1+2)}^0}{\partial x_2} \right)_{T,p} = b + 1,5cx_1^{0.5} + 2dx_1 + 2.5ex_1^{1.5} \quad (21)$$

Q and $RT \kappa_T$ values for {ethanol (1) + water (2)} binary mixtures, as well as the partial molar volumes of ethanol (1) and water (2), at the three temperatures considered here, were taken from the literature [22, 38, 39].

Otherwise, partial molar volumes of nonelectrolyte drugs are not frequently reported in the literature. This is because of the large uncertainty obtained in its determination due to their low solubilities, in particular in aqueous media. For this reason, in the first approach, the molar volume of triclin was considered as independent of co-solvent composition and temperature, as they are calculated according to the groups contribution method proposed by Fedors [29]. On the other hand, the radius of the drug molecule was calculated by using equation 8, as $r_3 = 0.407$ nm.

In order to apply the IKBI method, the correlation volume was iterated three times by using the equations (1), (7) and (9) to obtain the final values reported in Table 3. This property is almost independent on temperature in water-rich mixtures but increases to some extent in ethanol-rich mixtures. This would be expectable according to the variation of the respective molar expansibilities with the mixtures composition [40].

Table 3. Correlation volume ($\text{cm}^3 \text{mol}^{-1}$) for triclin in {ethanol (1) + water (2)} co-solvent mixtures at several temperatures after three iterations.

x_1	293.15 K	298.15 K	303.15 K	308.15 K	313.15 K
0.00	790.74	791.26	791.60	792.09	792.87
0.10	814.11	810.66	808.86	812.33	813.15
0.20	938.40	939.33	941.50	944.50	946.85
0.30	1033.69	1036.60	1039.18	1041.04	1043.50
0.40	1115.76	1118.16	1119.75	1122.04	1124.45
0.50	1196.96	1197.75	1198.42	1202.63	1205.53
0.60	1281.26	1280.71	1281.36	1288.19	1292.30
0.70	1363.04	1364.41	1367.61	1376.55	1383.36
0.80	1428.86	1435.71	1443.43	1451.91	1462.05
0.90	1485.75	1493.95	1501.84	1507.52	1516.46
1.00	1560.82	1566.06	1571.22	1576.68	1582.68

The preferential solvation parameter, $\delta x_{1,3}$ for ethanol (1) around triclin (3) is displayed in Fig. 4 at five temperatures. The values of $\delta x_{1,3}$ vary non-linearly with the proportion of ethanol (1) in the alcoholic mixtures (figure 4). The addition of ethanol to water causes a negative change in $\delta x_{1,3}$ from pure water (2) up to the 0.20 in molar fraction of ethanol (1) reaching minimum values near to -0.08 at 0.05 in molar fraction of ethanol at 303.15 K. In this composition, water is preferred over ethanol around the triclin (3), this because possibly the structuring of water molecules around the non-polar groups of this drug leading to hydrophobic hydration of the aromatic and methyl groups (Fig.1), contributes to lowering of the net $\delta x_{1,3}$ to negative values in these water-rich mixtures. This behavior is observed at all study temperatures as can be seen in Table 4. Although, a clear influence of the temperature in water-rich mixtures is not perceived, in ethanol-rich mixtures the solvation by ethanol increases with the increase in temperature what matches the solubility profile.

Table 4. $\delta x_{1,3}$ values of triclin (3) in {ethanol (1) + water (2)} co-solvent mixtures at several temperatures.

x_1	293.15 K	298.15 K	303.15 K	308.15 K	313.15 K
0.00	0.000	0.000	0.000	0.000	0.000
0.10	-0.070	-0.075	-0.078	-0.075	-0.075
0.20	-0.012	-0.013	-0.013	-0.012	-0.012
0.30	0.010	0.011	0.010	0.009	0.009
0.40	0.016	0.015	0.013	0.012	0.011
0.50	0.022	0.019	0.015	0.016	0.015
0.60	0.034	0.027	0.023	0.028	0.027
0.70	0.043	0.038	0.037	0.044	0.046
0.80	0.032	0.034	0.039	0.044	0.051
0.90	0.009	0.014	0.018	0.019	0.023
1.00	0.000	0.000	0.000	0.000	0.000

In the mixtures with composition $0.25 < x_1 < 1.00$, the local mole fraction of ethanol is greater than the one in the bulk and it increases with the temperature increasing. In this way, the co-solvent action may be related to the breaking of the ordered structure of water (hydrogen bonds) around the nonpolar moieties of the drug which increases the solvation of the triclin and has a maximum value near to $x_1 = 0.75$, i.e. $\delta x_{1,3} = 0.052$. On the other hand, although, as mentioned above, the maximum solubility was not achieved in a cosolvent mixture, what would be expected theoretically, the maximum

solvation is achieved in mixtures with polarities similar to those of triclin (3), this factor could also be involved in these behaviors.

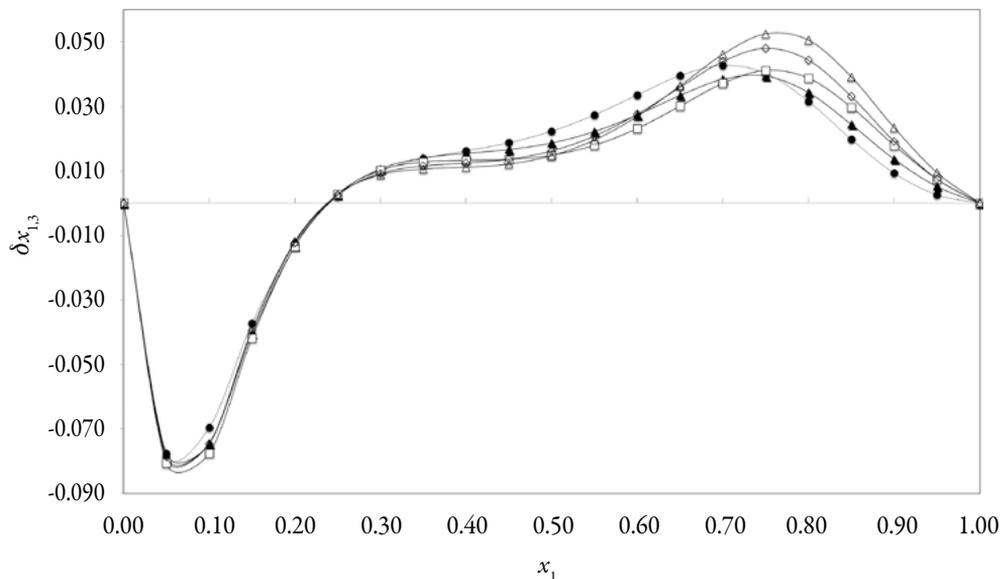


Figure 4. $\delta x_{1,3}$ values triclin (3) in {ethanol (1) + water (2)} co-solvent mixtures at several temperatures. (●=293.15 K; ▲=298.15 K; □=303.15 K; ◇=308.15 K; △=313.15 K).

The triclin (3) could act in solution as Lewis acids due to the hydrogen atom in their –OH groups in order to establish hydrogen bonds with proton-acceptor functional groups in EtOH and water (oxygen atom in –OH). In addition, these drugs could act as Lewis bases due to free electron pairs in oxygen atoms of hydroxyl and alkoxy groups to interact with hydrogen atoms present in both solvents. In this context, triclin has three hydrogen-bonding donor and seven hydrogen-bonding acceptor groups.

According to the preferential solvation results, it is conjecturable that in intermediate composition mixtures and ethanol-rich mixtures, triclin (3) is acting as Lewis acids with the ethanol molecules because this co-solvent is more basic than water as indicated by the Kamlet-Taft hydrogen bond acceptor parameters (β), i.e. 0.75 for ethanol (1) and 0.47 for water (2) [41,42]. In this way, triclin would prefer ethanol (1) instead of water. This behavior is similar to that presented by other drugs in aqueous cosolvent systems [27, 43, 44].

CONCLUSIONS

Explicit expressions for local mole fraction of ethanol and water around of triclin were derived on the basis of the IKBI method applied to equilibrium solubility values of this drug in {ethanol (1) + water (2)} mixtures. According to the performed analyses, triclin is preferentially solvated by water (2) in water-rich mixtures but preferentially solvated by ethanol (1) in mixtures with intermediate composition and those rich in ethanol at all temperatures considered.

DISCLOSURE STATEMENT

No potential conflict of interest was reported by the authors.

REFERENCES

1. H. Cai, M. Al-Fayez, R.G. Tunstall, S. Platton, P. Greaves, W.P. Steward, A.J. Gescher, The rice bran constituent triclin potently inhibits cyclooxygenase enzymes and interferes with intestinal carcinogenesis in ApcMin mice, *Mol. Cancer Ther.*, **4**, 1287-1292 (2005).
2. T. Oyama, Y. Yasui, S. Sugie, M. Koketsu, K. Watanabe, T. Tanaka, Dietary triclin suppresses inflammation-related colon carcinogenesis in male Crj: CD-1 mice, *Cancer Prev. Res.*, **2**, 1031-1038 (2009).
3. M. Li, Y. Pu, C.G. Yoo, A.J. Ragauskas, The occurrence of triclin and its derivatives in plants, *Green Chem.*, **18**, 1439-1454 (2016).
4. V.A. Moscatelli, Química y farmacología de una planta medicinal argentina: *Artemisia copa*, *Dominguezia*, **31**, 5-13 (2015).
5. A. Moheb, M. Grondin, R.K. Ibrahim, R. Roy, F. Sarhan, Winter wheat hull (husk) is a valuable source for triclin, a potential selective cytotoxic agent, *Food Chem.*, **138**, 931-973 (2013).
6. W. Lan, J. Rencoret, F. Lu, S.D. Karlen, B.G. Smith, P.J. Harris, J.C. del Rio, J. Ralph, Triclin-lignins: Occurrence and quantitation of triclin in relation to phylogeny, *Plant J.*, **88**, 1046-1057 (2016).
7. A. Jouyban, W.E. Acree, Mathematical derivation of the Jouyban-Acree model to represent solute solubility data in mixed solvents at various temperatures, *J. Mol. Liq.*, **256**, 541-547 (2018).

8. N.A. Bowden, D. Méndez-Sevillano, J.P.M. Sanders, M.E. Bruins, Modelling the effects of ethanol on the solubility of the proteinogenic amino acids with the NRTL, Gude and Jouyban-Acree models, *Fluid Phase Equilib.*, **459**, 158-169 (2018).
9. M.A. Kalam, A.A. Khan, A. Alshamsan, A. Haque, F. Shakeel; Solubility of a poorly soluble immunosuppressant in different pure solvents: Measurement, correlation, thermodynamics and molecular interactions, *J. Mol. Liq.*, **249**, 53-60 (2018).
10. E. Rahimpour, M. Barzegar-Jalali, A. Shayanfar, A. Jouyban, Generally trained models to predict drug solubility in N-methyl-2-pyrrolidone + water mixtures at various temperatures, *J. Mol. Liq.*, **254**, 34-38 (2018).
11. A. Fathi-Azarbayjani, M.A. Jalil-Vaez-Gharamaleki, A. Jouyban, Measurement and correlation of deferiprone solubility: Investigation of solubility parameter and application of van't Hoff equation and Jouyban–Acree model, *J. Mol. Liq.*, **215**, 339-344 (2016).
12. M.A. Ruidiaz, D.R. Delgado, C.P. Mora, A. Yurquina, F. Martínez, Estimation of the indomethacin solubility in ethanol + water mixtures by the extended Hildebrand solubility approach, *Rev. Colomb. Cienc. Quím. Farm.*, **39**, 79-95 (2010).
13. Y. Cheng, Z. Wang, S. Ding, J. Li, Determination and correlation of the solubility of triclin in water and ethanol mixtures, *J. Chem. Thermodyn.*, **89**, 89-92 (2015).
14. G. Chen, J. Chen, C. Cheng, Y. Cong, C. Du, H. Zhao, Solubility and preferential solvation of econazole nitrate in binary solvent mixtures of methanol, ethanol and 1,4-dioxane in water, *J. Chem. Thermodyn.*, **111**, 228-237 (2017).
15. J. Chen, G. Chen, Y. Cong, C. Du, H. Zhao, Solubility modelling and preferential solvation of paclobutrazol in co-solvent mixtures of (ethanol, n-propanol and 1,4-dioxane) + water, *J. Chem. Thermodyn.*, **112**, 249-258 (2017).
16. A. Jouyban, W.E. Acree Jr., F. Martínez, Modeling the solubility and preferential solvation of gallic acid in cosolvent + water mixtures, *J. Mol. Liq.*, **224**, 502-506 (2016).
17. Y. Marcus, “Solvent Mixtures: Properties and Selective Solvation”, Marcel Dekker, Inc., New York, 2002.
18. Y. Marcus, Preferential solvation of ibuprofen and naproxen in aqueous 1,2-propanediol, *Acta Chim. Slov.*, **56**, 40-44 (2009).

19. Y. Marcus, On the preferential solvation of drugs and PAHs in binary solvent mixtures, *J. Mol. Liq.*, **140**, 61-67 (2008).
20. D.I. Caviedes Rubio, R.G. Sotomayor, D.R. Delgado, Solvatación preferencial de la naringina en mezclas cosolventes etanol + agua mediante el método de las integrales inversas de Kirkwood-Buff, *Rev. Colomb. Cienc. Quím. Farm.*, **44**, 220-235 (2015).
21. D.R. Delgado, E.F. Vargas, F. Martínez, Preferential solvation of xylitol in ethanol + water solvent mixtures according to the IKBI and QLQC methods, *Rev. Colomb. Quím.*, **42**, 59-66 (2013).
22. D.R. Delgado, F. Martínez. Solubility and preferential solvation of sulfadiazine in methanol + water mixtures at several temperatures, *Fluid Phase Equilib.*, **379**, 128-138 (2015).
23. D.R. Delgado, M.A. Peña, F. Martínez, Preferential solvation of some sulfonamides in propylene glycol + water solvent mixtures according to the IKBI and QLQC methods, *J. Solution Chem.*, **43**, 360-374 (2014).
24. D.R. Delgado, M.Á. Peña, F. Martínez, Preferential solvation of acetaminophen in ethanol + water solvent mixtures according to the inverse Kirkwood-Buff integrals method, *Rev. Colomb. Cienc. Quím. Farm.*, **42**, 298-314 (2013).
25. A.C. Gaviria-Castillo, J.D. Artunduaga-Tole, J.D. Rodríguez-Rubiano, J.A. Zúñiga-Andrade, D.R. Delgado, A. Jouyban, F. Martínez, Solution thermodynamics and preferential solvation of triclocarban in {1, 4-dioxane (1) + water (2)} mixtures at 298.15 K, *Phys. Chem. Liq.*, Forthcoming 2018, doi: 10.1080/00319104.2017.1416613.
26. J.A. Lasso, D.I. Caviedes, D.R. Delgado, Preferential solvation of 4-hydroxy-2,5-dimethyl-3(2H)-furanone (DMHF) in ethanol + water mixtures according to IKBI and QLQC methods, *Ingeniería y Región*, **13**, 139-147 (2015).
27. A. Jouyban, S. Nozohouri, F. Martínez, Solubility of celecoxib in {2-propanol (1) + water (2)} mixtures at various temperatures: Experimental data and thermodynamic analysis *J. Mol. Liq.*, **254**, 1-7 (2018).
28. A.F.M. Barton, "Handbook of Solubility parameters and Other Cohesion Parameter", 2nd edition, CRC Press, Inc., New York, 1991.
29. R.F. Fedors, A method for estimating both the solubility parameters and molar volumes of liquids, *Polym. Eng. Sci.*, **14**, 147-154 (1974).

30. D.M. Jimenez, Z.J. Cárdenas, D.R. Delgado, M.Á. Peña, F. Martínez, Solubility temperature dependence and preferential solvation of sulfadiazine in 1,4-dioxane + water co-solvent mixtures, *Fluid Phase Equilib.*, **397**, 26-36 (2015).
31. D.R. Delgado, A.R. Holguín, O.A. Almanza, F. Martínez, Y. Marcus, Solubility and preferential solvation of meloxicam in ethanol + water mixtures, *Fluid Phase Equilib.*, **305**, 88-95 (2011).
32. D.R. Delgado, F. Martínez, Solubility and preferential solvation of sulfadiazine in methanol + water mixtures at several temperatures, *Fluid Phase Equilib.*, **379**, 128-138 (2014).
33. D.R. Delgado, F. Martínez, Solubility and solution thermodynamics of sulfamerazine and sulfamethazine in some ethanol + water mixtures, *Fluid Phase Equilib.*, **360**, 88-96 (2013).
34. E.A. Ahumada, D.R. Delgado, F. Martínez. Solution thermodynamics of acetaminophen in some PEG 400 + water mixtures, *Fluid Phase Equilib.*, **332**, 120-127 (2012).
35. D.R. Delgado, F. Martínez. Solution thermodynamics of sulfadiazine in some ethanol + water mixtures, *J. Mol. Liq.*, **187**, 99-105 (2013).
36. D.R. Delgado, F. Martínez. Solubility and solution thermodynamics of some sulfonamides in 1-propanol + water mixtures, *J. Solution Chem.*, **43**, 836-852 (2014).
37. E.A. Cantillo, D.R. Delgado, F. Martínez, Solution thermodynamics of indomethacin in ethanol + propylene glycol mixtures, *J. Mol. Liq.*, **181**, 62-67 (2013).
38. D.R. Delgado, F. Martínez, Preferential solvation of sulfadiazine, sulfamerazine and sulfamethazine in ethanol + water solvent mixtures according to the IKBI method, *J. Mol. Liq.*, **193**, 152-159 (2014).
39. D.M. Jiménez, Z.J. Cárdenas, D.R. Delgado, F. Martínez, A. Jouyban, Preferential solvation of methocarbamol in aqueous binary cosolvent mixtures at 298.15 K, *Phys. Chem. Liq.*, **52**, 726-737 (2014).
40. J. Jiménez, J. Manrique, F. Martínez, Effect of temperature on some volumetric properties for ethanol+ water mixtures, *Rev. Colomb. Cienc. Quím. Farm.*, **33**, 145-155 (2004).

41. M.J. Kamlet, R.W. Taft, The solvatochromic comparison method. I. The beta-scale of solvent hydrogen-bond acceptor (HBA) basicities, *J. Am. Chem. Soc.*, **98**, 377-383 (1976).
42. R.W. Taft, M.J. Kamlet, The solvatochromic comparison method. II. The alpha-scale of solvent hydrogen-bond donor (hba) acidities, *J. Am. Chem. Soc.*, **98**, 2886-2894 (1976).
43. F. Martínez, A. Jouyban, W.E. Acree Jr., Further numerical analysis on the solubility of ibrutinib in ethanol + water mixtures at different temperatures, *J. Mol. Liq.*, **218**, 35-38 (2016).
44. A. Jouyban, F. Martínez, W.E. Acree Jr., Comments on "Solubility and solution thermodynamics of 2,3,4,5-tetrabromothiophene in (ethanol + trichloromethane) binary solvent mixtures", *Fluid Phase Equilib.*, **421**, 88-92 (2016)..

HOW TO CITE THIS ARTICLE

J.J. Sandoval-Castro, C.P. Ortiz, J.D. Rodríguez-Rubiano, G.A. Rodríguez-Rodríguez, D.R. Delgado, Preferential solvation of triclin in {ethanol (1) + water (2)} mixtures at several temperatures, *Rev. Colomb. Cienc. Quím. Farm.*, **47**(2), 135-149 (2018).

